

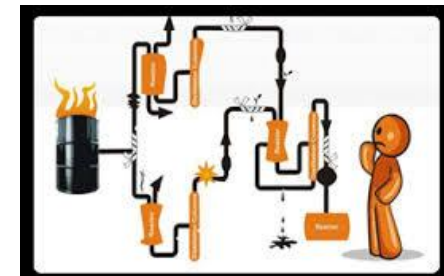
PROCESS HAZARDS ANALYSIS

PHA

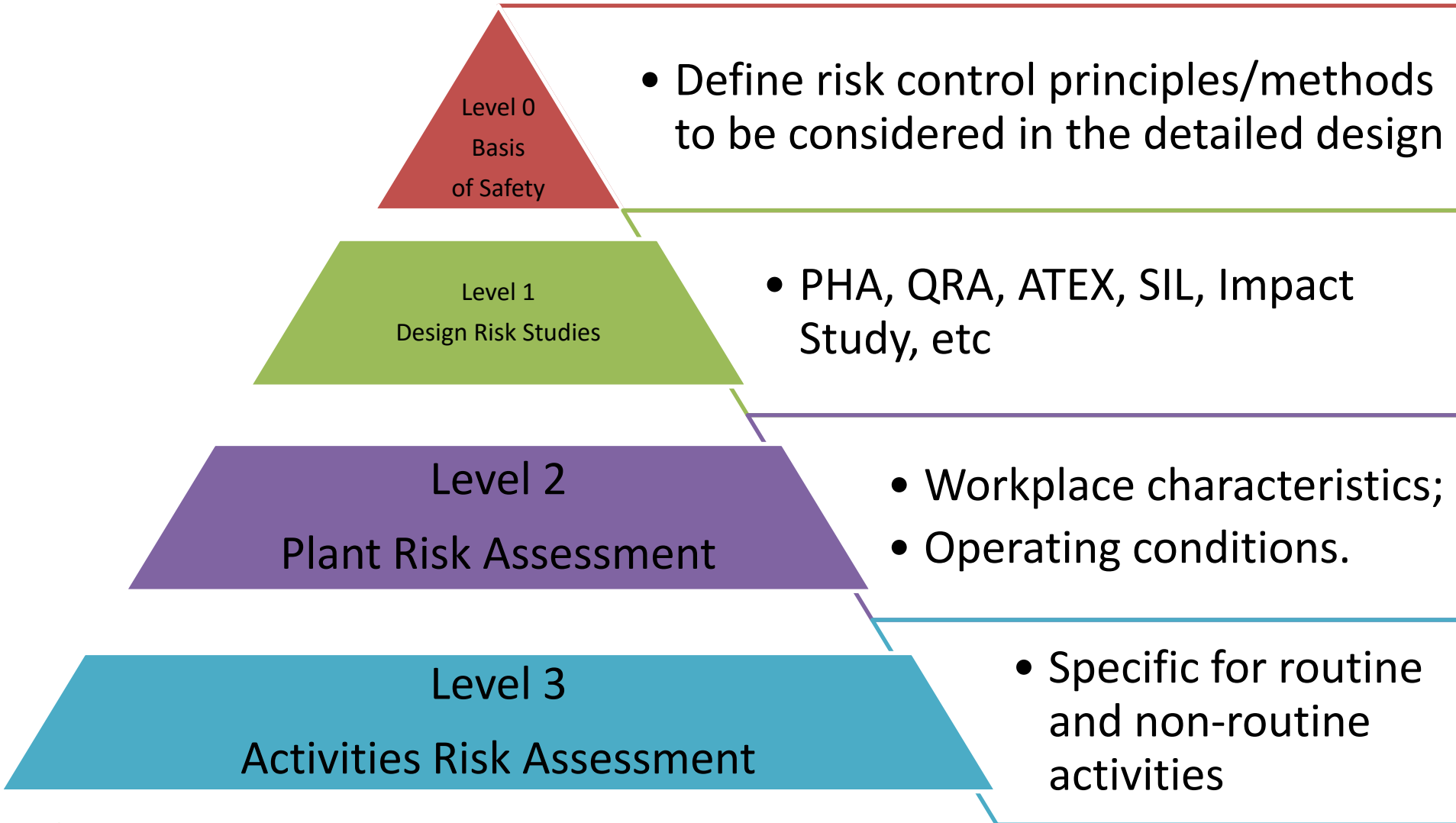
THEODOROS KRANIDIOTIS
MANAGEMENT FORCE GROUP

What is PHA?

- Proactive and systematic identification and evaluation of “incidents” that could occur as a result of failures in process, procedures or equipment;
- It provides the structure upon which an effective Process Safety Management program is designed and built;
- It is applied during the detailed design of a Project and before applying a “design change” during normal operation.



Risk Control Pyramid



Why PHA?



- Legal compliance:
 - Prevent incidents;
 - SEVESO regulated facilities; HP NG systems;
- Business optimization:
 - Less interruption, no loss of production, increased productivity, higher turnover/profit.
- Costs saving:
 - Insurance;
 - Cheaper/sometimes only possible to intervene during design than later.
- Corporate image:
 - Less problems with authorities, no incidents;
 - Easier permitting;
 - Easier investment, market more accessible to good performers.

PHA Objective

- Identify hazards as early as possible, in order to determine the most appropriate “solution” for managing their risk;
- Modifications made early in the design stage of project have minimal effect on cost and schedule;
- PHA methodology shall be appropriate to the complexity of the process.



The PHA Must Address

- Facilities description/sitting.
- Components/Equipment in the process;
- Hazards of the process;
- Consequences of deviations or failures;
- Engineering and administrative controls;
- Human factors;
- Evaluation of consequences and effects;
Qualitative/Semi-Quantitative;
- Steps required to correct or avoid failures/deviations.

ID	DEVIATION	CAUSES	CONSEQUENCES	SAFEGUARDS	S. L. R.	RFFR	RECOMMENDATION
1.1	No flow	Control valve CV-22 fails	1.1.1 Information to production location due to production flow from adjacent causing control systems to shut down process 1.1.2 Potential overpressure of CV-22 piping if failed, closed piping heats up	1.1.1 Filling closed, or accidentally closing 1.1.2 Single valve are provided for the section (off-line piping between V-100 and V-101) 1.1.3 Filling closed, or accidentally closing 1.1.4 Filling closed, or accidentally closing 1.1.5 Filling closed, or accidentally closing	4	10	No recommendation
2	Control system incorrectly activates shutdown by "fault" condition	Potential overpressure of CV-22 piping if failed, closed piping heats up	2.1.1 Potential overpressure of CV-22 piping if failed, closed piping heats up 2.1.2 Potential overpressure of CV-22 piping if failed, closed piping heats up 2.1.3 Filling closed, or accidentally closing 2.1.4 Filling closed, or accidentally closing	2.1.1 Filling closed, or accidentally closing 2.1.2 Single valve are provided for the section (off-line piping between V-100 and V-101) 2.1.3 Filling closed, or accidentally closing 2.1.4 Filling closed, or accidentally closing	4	10	2.1.5 "Isolated gate to the rupture disk" inspection being performed within 24h of the rupture disk
3	Control valve closed due to incorrect logic or setting	Control valve closed due to incorrect logic or setting	3.1 Information to production location due to production flow from adjacent causing	3.1 Filling closed, or accidentally closing 3.2 Single valve are provided for the section (off-line piping between V-100 and V-101)	4	10	No further recommendation

PHA Methodologies

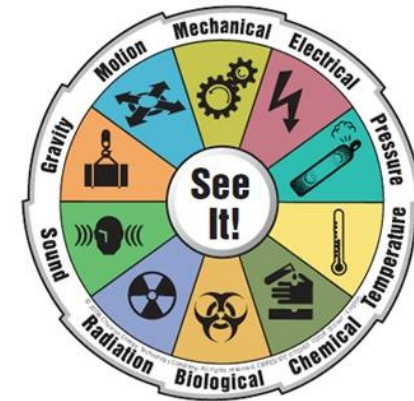
- Hazard and Operability – HAZOP;
- Hazard Identification – HAZID;
- What-If analysis;
- Checklists;
- Failure Mode and Effects Analysis –FMEA;
- Fault Tree Analysis;
- Combination of the above.

HAZID/HAZOP

- PHA methodology presented includes:
 - **Hazard Identification (HAZID):** A structured approach for the identification of undesirable consequences (human, environment, business). Usually a register of all possible hazards is considered.
 - **Hazard and Operability study (HAZOP):** A systematic approach to identify hazards and operability problems occurring a result of deviations from the intended range of process conditions;

HAZID

- Team work:
 - Chairman, Safety, Operation, Maintenance, Designer, Other.
- Review of physical hazards and operability issues associated with the facilities;
- Process and human interaction is considered;
- Project is divided into manageable, logical sections (systems or units);
- Team analyzes each section using a proposed register of hazards and consequences and identifies which hazards can be realized and what are their consequences.



HAZID Register (ISO 17776)

- Natural Hazards:
 - Temperature extremes, Waves, Wind, Dust, etc.
- External & 3rd Party Hazards:
 - Sabotage, Third Party Activities, etc.
- Facility Systems:
 - Hydrocarbons under pressure, Toxics, Liquids and gases under high pressure, Hot or cryogenic fluids, Blastic agents, Explosives, Dangerous equipment, Ignition sources, Lifting facilities, Health Hazards, Working Environment, etc.

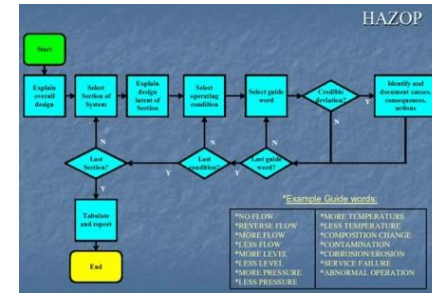
HAZID

- Once the hazards applicable are identified, an assessment for each hazard is made:
 - **Raw Risk:** is the risk introduced in a system without considering the safeguards according to the design.;
 - **Residual Risk:** is the residual risk estimated considering the safeguards defined in the design. If residual risk is still intolerable then recommendations shall be considered;
 - **Final Risk:** is the risk estimated considering the proposed recommendation(s).

Risk Ranking

		Likelihood				
		1-Very Unlikely ($<10^{-6}$)	2- Unlikely (10^{-6} to 10^{-4})	3- Likely (10^{-4} to 10^{-2})	4- Very likely (10^{-2} to 10^{-1})	5- Certain (10^{-1} to 1)
Severity	5-Catastrophic Internal: many fatalities External: irreversible effects, multiple fatalities	5	10	15	20	25
	4-Very Extensive Internal: Fatality. External: irreversible effects, fatality, public evacuation	4	8	12	UNACCEPTABLE	
	3-Critical Internal: major injuries. External: irreversible effects, public shelter in place	6	9	12		
	2-Marginal Internal: small injury. External: reversible effects	ACCEPTABLE		4	8	10
	1-Negligible Internal: First aid, keep working. External: no effects			1	3	4

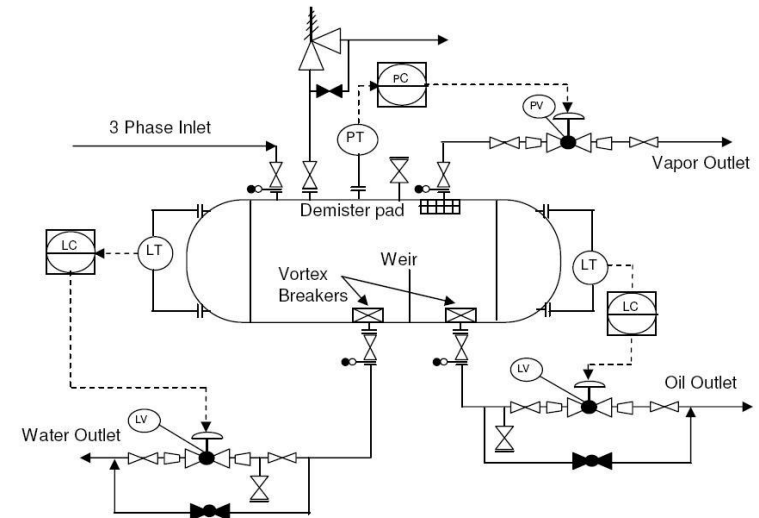
HAZOP



- Team Work:
 - Chairman, Process, Safety, Operation, Maintenance, Instrument, Other.
- Systems/processes are divided into nodes;
- Each node systems/components is systematically questioning in order to establish how deviations from the design intent can arise;
- Appropriate guidewords and deviations are used to focus the attention of the team upon deviations and their possible causes.

HAZOP Guide Words

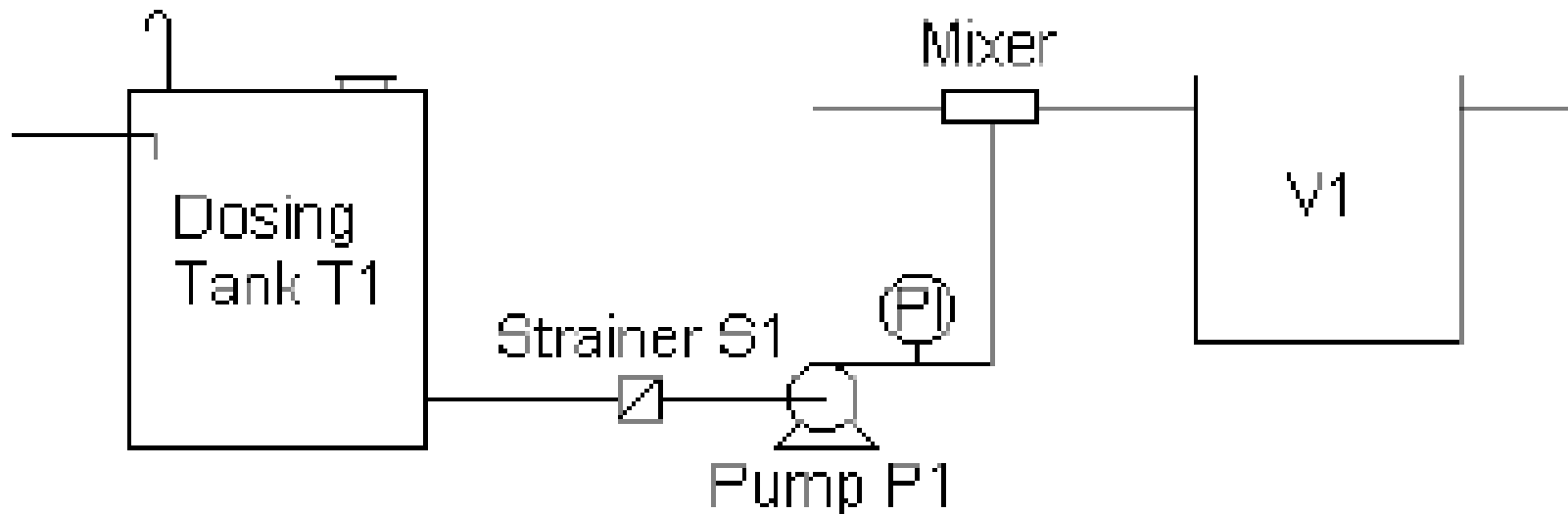
- Flow
 - Low/No/High/ Reverse
- Pressure
 - Low/High
- Level
 - Low/High
- Temperature
 - Low/High
- Different Composition / Contamination
- Corrosion/Erosion/Deposition
- Loss of power / utilities / instrumentation
- Isolation / Drain / Vent
- Start-up / Shut down
- Other



HAZOP

- Once a deviation is considered valid, consequences are identified and an assessment is made according to the risk assessment approach (Raw Risk, Residual Risk, Final Risk);
- If “Residual Risk” is still “Intolerable” recommendations are raised for further actions;
- Typical assumptions:
 - No catastrophic loss, No double jeopardy, Good faith

Analysis Example



Deviation

No Flow

Cause

Strainer S1 blockage due to impurities in Dosing Tank T1

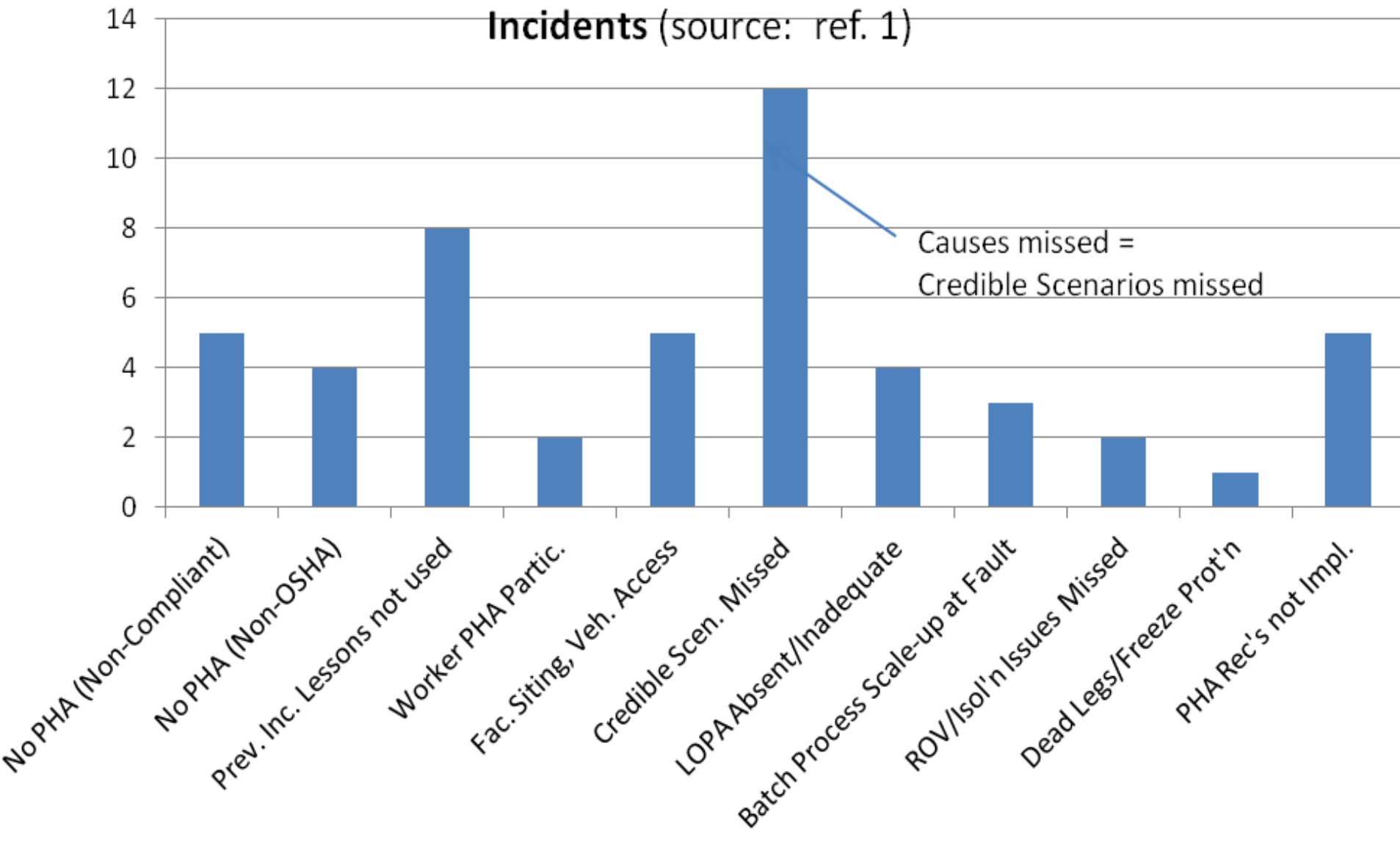
Consequences

- Tank T1 High level, overflow, injury, fire/toxic
- Cavitation in Pump P1, pump damage
- Loss of process

Always be Alert

- PHA may not identify all incidents that could occur in a process if:
 - A scenario may be excluded from the scope of the analysis;
 - The team may be unaware of a scenario;
 - The team consider the scenario but judge it not credible or significant;
 - The team may overlook the scenario.
- No shortcuts; systematic consideration;
- PHA team experience and expertise.

Figure 1. Pareto Analysis: Contributing Factors to Serious Incidents (source: ref. 1)



Mark Kaszniak, —Oversights and Omissions in Process Hazard Analyses: Lessons Learned from CSB InvestigationsII, presented at the AIChE 2009 Spring National Meeting, 5th Global Congress on Process Safety, 43rd Annual Loss Prevention Symposium, Tampa, Florida (April 26–30, 2009)

Summary

- The Process Hazard Analysis is the backbone of the Process Safety Management program;
- PHA is the tool to achieve:
 - Risk reduction;
 - Business optimization.
- Questions?
- Contact Details: Theodoros Kranidiotis,
tkranidiotis@mforsafety.com, +30 6947709950